Spring 2021

# 控制系統 Control Systems

## Unit 4D Ziegler–Nichols Tuning

Feng-Li Lian NTU-EE

Feb – Jun, 2021

- Callender, Hartree, Porter (1936) proposed a design for PID controllers by specifying satisfactory values for the terms based on estimates of the plant parameters that an operating engineer could make from experiments on the process.
- Extended by Ziegler and Nichols (1942, 1943) who recognized that the step response of a large number of process control systems exhibit a process reaction curve,

generated from experimental step response data.



$$\frac{Y(s)}{U(s)} = \frac{A e^{-s t_d}}{\tau s + 1}$$

 A first-order system with a time delay (lag)

### Ziegler–Nichols Tuning of the PID Controller

## Method 1:

In a closed-loop step response transient with a decay ratio of 0.25

$$D_c(s) = k_P \left( 1 + \frac{1}{T_I s} + T_D s \right)$$

#### • Quarter decay ratio



#### Ziegler–Nichols Tuning for the Regulator $D_c(s) = k_P(1 + 1/T_I s + T_D s)$ , for a Decay Ratio of 0.25

Type of Controller	Optimum Gain
Р	$k_P = 1/RL$
PI	$\begin{cases} k_P = 0.9/RL \\ T_I = L/0.3 \end{cases}$
PID	$\begin{cases} k_P = 1.2/RL \\ T_I = 2L \\ T_D = 0.5L \end{cases}$

Method 2: Ultimate Sensitivity Method:

Based on evaluating the amplitude and frequency

of the oscillations of the system at the limit of stability

rather than on taking a step response.



#### **Examples**

- Example 4.8: Tuning of a Heat Exchanger: Quarter Decay Ratio
- The measured process reaction curve
- Maximum slope: R = 1/90
- Time delay: L = 13 sec
- = 1/RL = 90/13 = 6.92• P:  $K_{P}$
- PI:  $K_P$ = 0.9/RL





• and  $T_{I}$ 

= L/0.3

= 13/0.3 = 43.3





**A** 

#### Examples

